GPAC/PJVA Joint Conference

CO₂ Dehydration: Why? How Much? How?

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Never take your eye off the target



Section 1

Who Are We?

Who?

Acid Gas Injection

- Oil & gas EPCM company formed in 1987 currently employ 250 people
- Started acid gas injection early first project was in 1995
- Worked on acid gas projects or provided training in 12 countries outside of Canada, including 6 states in the US
- Involved in about 25% of the Alberta acid gas injection projects to date
- Published 7 books and over 50 articles and technical papers relevant to acid gas and CO₂ behavior, facility design, and injection operational issues
- Patented a novel cost effective acid gas dehydration process

Why? How Much ? How ?

Section 2

Why Dehydrate?

3 Reasons

Corrosion Hydrate Formation Imposed Specs

Corrosion





+

= ACID !

Corrosion

IT IS ALL ABOUT THE CONTAMINANTS

- carbonic, sulfuric, and nitric acids will form where CO₂, SO₂, and NO_x are present
- excess oxygen allows the corrosion to continue
- most likely cause of off-spec water content is carry over of water/glycol from the dehydration process
- stainless steel piping alternative is ~4-5 times more expensive than mild steel

Table 6-9 Corrosion of Mild Steel by Carbon Dioxide and Other Gases in Water*						
Gas Concentration, ppm		Corrosion of Mild Steel, mils/year A: CO ₂ conc. 200 ppm B: CO ₂ conc. 600 ppm				
<u> </u>		20				
8.8	0	28	60			
4.3	0	18	44			
1.6	0	12	34			
0.4	0	17	27			
< 0.5	35	6	6			
<0.5	150	15	16			
< 0.5	400	17	21			



*Temperature 80°F, exposure time 72 hr.

Source: Data of Watkins and Kincheloe (1958) and Watkins and Wright (1953)

Gas Purification, 5th edition

Hydrates

Definition

A physical combination of water and small molecules producing a crystalline compound having "ice like" appearance but possessing different properties and structure than ice.

Problem

At some temperature, above the freezing point of water, the water and acid gas will begin to form a solid called a hydrate.

The Hydrate Formation Temperature and varies according to the pressure, gas composition, and water content of the vapour.

Hydrates cause reduced heat transfer, excess pressure drops, blockages, and safety concerns.





Hydrate Formation



Pipeline Spec

 CO₂ pipeline operators impose minimum quality requirements for corrosion control and hydrate prevention

Kinder Morgan CO₂ Pipeline Spec (June 5, 2008)

<u>Component</u>	<u>Standard</u>
Purity	95% mole percent of Carbon Dioxide
Water	no free water, not more than thirty (30) pounds of water per MMscf in the vapor phase
Oxygen	not more than ten (10) parts per million, by weight, of oxygen
Hydrogen Sulfide	not more than twenty (20) parts per million, by weight, of hydrogen sulfide
Total Sulfur	not more than thirty-five (35) parts per million, by weight, of total sulfur
Nitrogen	not more than four mole percent (4%) of nitrogen
Temperature	not exceed a temperature of 120°F
Hydrocarbons	not more than five mole percent (5%) of hydrocarbons; dew point not higher than -20°F
Other	not contain more than 0.3 (three tenths) gallons of glycol per MMcf and at no time shall such glycol be present in a liquid state at the pressure and temperature conditions of the pipeline

Pipeline Spec

DNV-RP-J202 - "Design and Operation of CO₂ Pipelines" (April 2010)

- 4.8.3 Limitations on water content
 - "... ensure that no free water may occur at any location in the pipeline within the operational and potential upset envelopes and modes, unless corrosion damage is avoided through material selection."
 - normal operation pressure and temperature envelope
 - safety factor of 2 is recommended
 - shut-in pressure combined with minimum ambient temperature
 - depressurization scenario
 - water dropout cannot be prevented without very stringent limits

Water content spec needs to be established according to the local transportation conditions

- Piping across the plant site might only require 75 lb/MMscf (1,580 ppm_v)
- Above ground piping in Arctic permafrost may require 12 lb/MMscf (252 ppm_v)

Section 3

How Much Dehydration ?

How Much?

Acid Gas Phase Envelopes



How Much?

Water Content - AQUAlibrium



How Much?

Water Content - AQUAlibrium



Section 4

How to Dehydrate ?

Methods

Compression

Water content in vapour is reduced as pressure is increased

Desiccant

- Absorption
 - solid calcium chloride
 - liquid glycerin, glycols (TEG)
- Adsorption gels, alumina, molecular sieve

Refrigeration – thermodynamic phase separation

- External (closed)
 - A/C, car, refrigerator, arena, gas plant liquids recovery
- Internal (auto-refrigeration)
 - Choke plant dew point control
 - DexPro[™] (patented)

Separation – 'mechanical' membrane permeation

Compression



Absorption

Simplified process overview - glycol

- CO₂ flows from the bottom up through a contactor
- 'dry' glycol flows from the top down through the contactor
- glycol absorbs water from the CO₂ as it flows through the glycol
- water, and other absorbed contaminants, are boiled out of the 'wet' glycol in a reboiler
- HIGH PRESSURE LOW PRESSURE REGENERATION SYSTEM CONTACTING SYSTEM VAPOR OUTLET (TCV) \Rightarrow (OPTIONAL) REFLUX GAS (LCV) SKIMMER SURGE (OPTIONAL) (LC) FUEL 10) ¥ (10) GAS INLET SCRUB-GAS/GLYCOL GLYCOL/GLYCOL HEAT EXCHANGER BER HEAT CONTACTOR SOCK CHANGE FILTER FILTER (OPTIONAL) TOWER CONDENSATE TO FREE DRY DRAIN LIQUID GAS OUTLET WET GAS INLET GLYCOL CIRCULATION PUMP
- 'dry' glycol is recycled back to the contactor

Absorption



Adsorption

Simplified process description - Molecular Sieve

- 'wet' CO₂ is dehydrated in one tower while the other tower is regenerating
- gas is heated up to 315 degC and reversed to regenerate the tower



Adsorption





Refrigeration - external

Simplified process description

- Condenser
 - refrigerant is condensed to liquid

Expansion

- liquid refrigerant is expanded across a JT valve to desired temperature
- Evaporator (chiller)
 - cold refrigerant absorbs heat from CO₂ and evaporates refrigerant
- Compressor
 - refrigerant vapour is recompressed to desired cycle pressure and returned to condenser



DexPro™

Simplified process description - DexPro™

- TCV or JTV (Joule-Thomson Valve)
 - Cools a small slip stream of Dry acid gas by reducing the pressure (expansion)
- DexPro[™] Module
 - Cold Dry Acid Gas mixes with Wet acid gas in the DexPro Module
- Stage 5 Suction Scrubber/Compressor/Cooler
 - Condensed water from the DexPro Module is removed in suction scrubber
 - Cool Dry acid gas increases fluid compression efficiency













Section 5

How do they Compare ?

Glycol & Molecular Sieve Dehydration – 49^oC



Refrigeration & DexPro™ – 49^oC



Compressor Performance vs. Inlet Temperature



Example Case

- 1,000 tonne/day \rightarrow 538,300 Sm³/d of dry CO₂
- water saturated at 48°C @ 40 kPa(g)
- pipeline inlet design pressure \rightarrow 13,800 kPa(g)
- 4 compression (centrifugal) stages
- inter-stage / after-cooling between compressor stages
 - 40°C process (CO₂)
- 632 ppm_v dehydration requirement (30 lb/MMscf)
 - ~-20°C hydrate formation temperature

Process

			No	Triethylene	External	D Due IM	
			Dehydration	Glycol	Refrigeration	DexPro™	
Compression	main	hp _{gas}	5,469.9	5,494.0	5,256.8	5,539.0	
	refrigeration	hp _{gas}			163.3		
		total	5,469.9	5,494.0	5,420.1	5,539.0	
				0.44%	-0.91%	1.26%	Horsepower
Cooling Water	main	gpm _{US}	1,441	1,446	1,340	1,447	
	condenser	gpm _{US}			94		
		total	1,441.0	1,446.0	1,434.0	1,447.0	Cooling
				0.35%	-0.49%	0.42%	Cooning
Heat	regenerator	btu/hr		80,257			Regeneration
Regenerator Vent	CO ₂	t/yr		135.2			
	Water	t/yr		280.6			Still Vent
	Glycol	lb/yr		41.0			
Glycol losses	pipeline	lb/yr		17,788.9			TEG lossos
	vent	lb/yr		41.0			TEGIOSSES
Methanol losses	pipeline	lb/hr			23.2		
		bbl/d			2.0		Weon iosses

Size

TEG Deh	y l	DexPro™	n	
	, Weight		Weight	
30" Contactor	6,500	DexPro™ Module	350	
Still Column	200	Regulators	10	
Vent	200	Analyzer	75	
Flash Tank	500	Control Panel	65	
Reboiler/Surge	1,000	Pump/motor	50	
Piping	1,450	Frame	75	
Skid	1,700	Instruments	50	
Wiring	200	Wiring	200	
Glycol	3,000			
miscellaneous	250	miscellaneous	125	
Total (kg.) 15,000		Total (kg.) 1,00		
tonne	15.0	tonne	1.0	Lowest Weig
	Size		Size	
Height	9.2 m.	Height	1.8 m.	
Length	4.3 m.	Length	1.8 m.	
Width	2.4 m.	Width	0.6 m.	
Footprint (m ²)	10.3	Footprint (m ²)	1.1	Lowest Area

Economics

		No	Triethylene	External	DevPro™	
		Dehydration	Glycol	Refrigeration	DEXITO	
Dehydration Capital Cost	installed	\$ -	\$ 2,100,000	\$ 1,350,000	\$ 600,000	Lowest CAPEX
Annual Operating Cost						
Compression	\$70/MWhr	\$ 2,502,206	\$ 2,513,218	\$ 2,479,409	\$ 2,533,788	
Triethylene Glycol	\$1.00/lb	\$ -	\$ 843	\$-	\$-	
Methanol	\$0.25/lb	\$ -	\$-	\$ 50,812	\$-	
Annual Maintenance Cost			\$ 210,000	\$ 135,000	\$ 6,000	4
Total Annual Cost		\$ 2,502,206	\$ 2,724,061	\$ 2,665,221	\$ 2,539,788	Lowest OPEX
Present Value of Operating Cost		\$ 26,508,403	\$28,858,740	\$28,235,388	\$26,906,550	
discount rate	7%					
term (years)	20					
	TOTAL NPV	\$ 26,508,403	\$30,958,740	\$29,585,388	\$27,506,550	
	difference	\$ -	\$ 4,450,337	\$ 3,076,986	\$ 998,147	Best NPV

♣ DexPro[™] capital cost does not reflect one time license fee

DexPro™

DexPro™ has a number of key advantages

- Lowest capital cost (CAPEX)
- Lowest operating cost (OPEX)
- Best economics (NPV)
- No rotating equipment
- Simplicity of process and equipment
- Extreme turndown
- No fugitive emissions or off-gas handling requirement
- Very small environmental footprint
- Very small physical footprint

QUESTIONS ?

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