

# Waste Heat Recovery Bigstone Plant Brian Deschner

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ENERGY

# Biography

- Employed with Talisman for 25 years
- Worked 14 years in Chauvin in Oilfield as Engineering Technologist, operated wells and batteries, optimized wells, managed downhole work and supervised service rigs
- The last 11 years have been focused in Edson area gas properties as an Operations Technologist
- Currently working in a role as Rotating Equipment Technologist
- Certified Engineering Technologist

# Agenda

- Background – Bigstone Plant
- WHRU Project Background and Purpose
- Waste Heat Recovery Unit Design
- Controls– Instrumentation and Logic
- Challenges
- Installation
- Final Pictures
- Summary --Benefits / Impacts
- Moving Forward– Future Considerations
- Questions



# Background - Bigstone Plant

- Plant was built in 1995 by Petromet Resources Ltd.
- Sweet gas plant at 14-28-59-22 W5M
- Licensed throughput of 80 mmcf/d sales and 85 mmcf/d raw
- Compression – 4 Reciprocating Inlet and 2 Solar Turbine Sales Compressors
- Starting looking at WHRU project in 2006, opportunity existed because of the need for additional heat in the process, installed in 2009

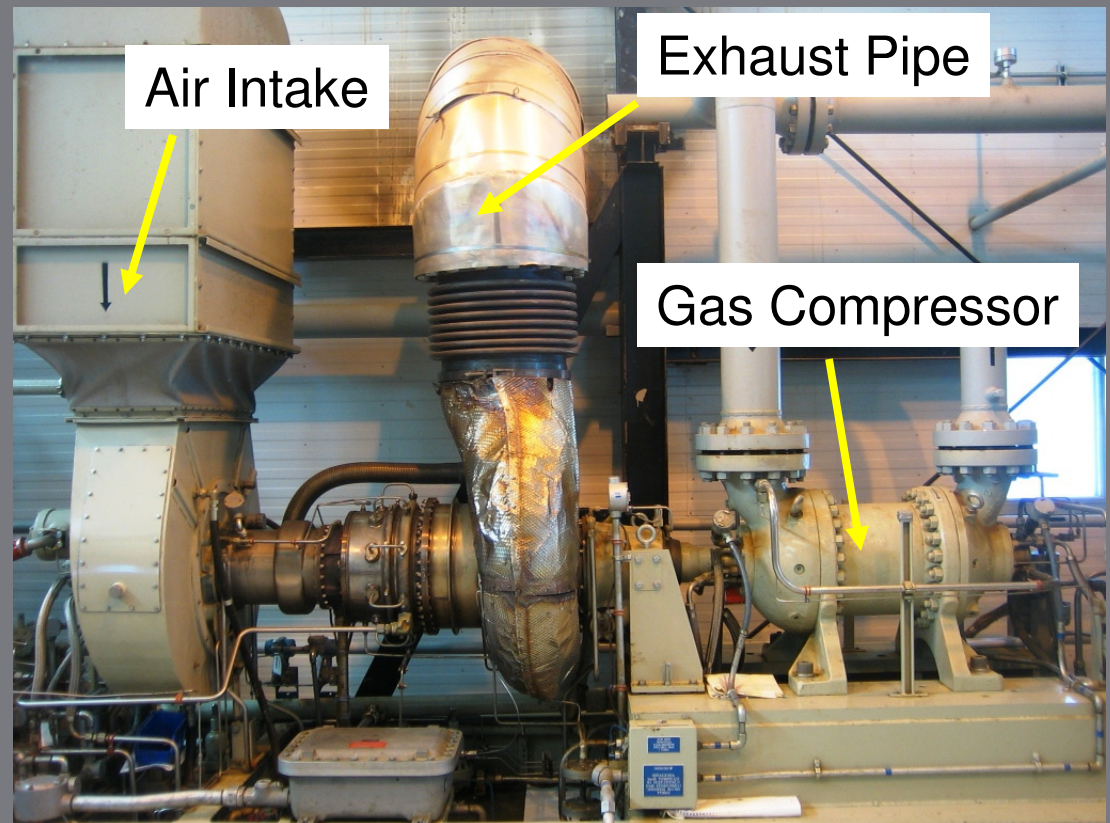
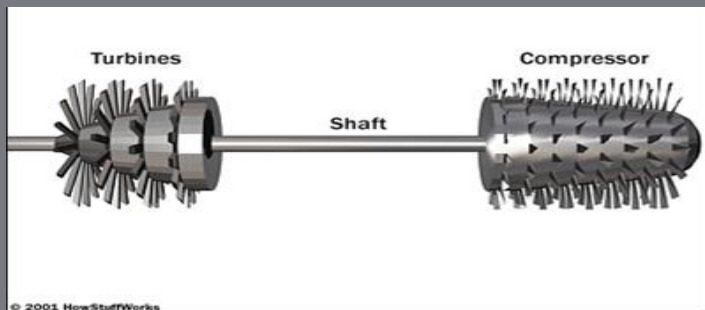
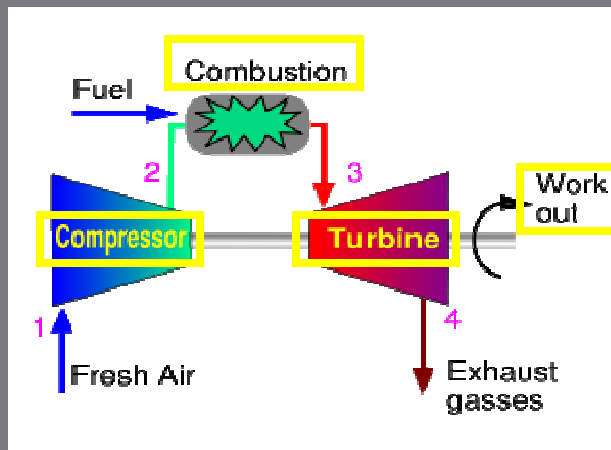


# WHRU Project Background

- Waste Heat Recovery Unit (WHRU):
  - Recovers waste heat from exhaust of sales compressors and use heat exchangers to heat process fluids
  - Replaces fired heaters in current heat systems
    - Hot Oil (Process)
    - Glycol (Heat tracing)
  - Fuel gas savings
  - Increases heat medium reliability
    - Glycol system was taxed

# WHRU Project Background--Turbines

- Saturn T1600 Solar Turbine Engine
  - Centrifugal compressor attached





# WHRU Project Background-- Turbines

- Outside view of Solar Turbine Building where WHRU was installed
- Replaced current exhaust stack with a dump stack and the WHRU (built into a second stack)
- Replaces fired heaters for hot oil and glycol (7.5 mm BTU/h)
- Excess heat is diverted up the dump stack



# WHRU Project Background

- Installation Site:
  - WHRU replaced existing exhaust stack
  - This stack provided easy access to pipe-rack
  - Existing hot oil heater and glycol heater were kept in line





# WHRU Design- Sales Compressors

- Engine Performance:

Engine Inlet Temp	10.0 °C
Driven Equipment Speed	22300 RPM
Net Output Power	987 kW
Heat Rate	15649 kJ/kWh
Inlet Air Flow	20994 kg/h
Engine Exhaust Flow	20215 kg/h
Exhaust Temperature	527 °C

- Heat Output                      11 mm BTU/h      (One Turbine Exhaust)

# WHRU Design-- Hot Oil Heater

- Design Conditions
  - Load 6.0 mm BTU/h
  - Inlet Temp 160 °C
  - Outlet Temp 180 °C
- Esso Thermoil-- Heat Transfer Oil 46
  - Max Temp 200 °C
- Fuel Gas Usage
  - Approx 175 mcf/d (6.0 mm BTU/hr)
- Heat Usage
  - Glycol reboiler to regenerate tri-ethylene glycol
  - De-ethanizer bottom and de-ethanizer reboiler to release light ends from condensate



# WHRU Design- Glycol Heater

- Design Conditions
  - Load 1.5 mm BTU/h
  - Inlet Temp 40 °C
  - Outlet Temp 80 °C
- 50/50 Ethylene Glycol – Water Mixture
- Fuel Gas Usage
  - Approx 125.0 mcf/d (1.5 mm BTU/h)
- Heat Usage
  - Building heat (roughneck heaters)
  - Heat Tracing (pipes and tanks)

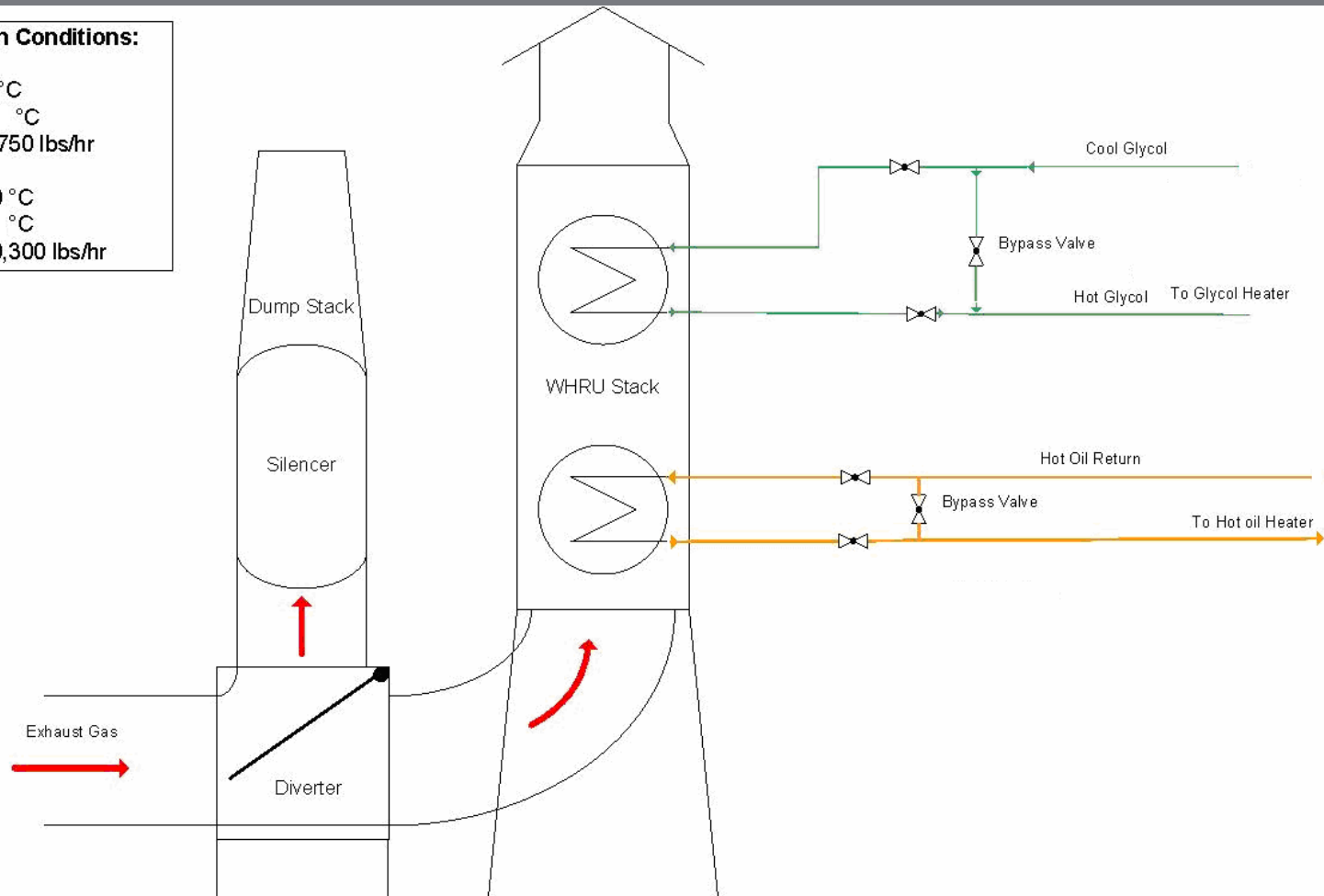


# WHRU Design – Initial Concept

## Proposed Design Conditions:

Glycol In = 40 °C  
Glycol Out = 79 °C  
Rate = 50,750 lbs/hr

Hot Oil In = 160 °C  
Hot Oil Out = 178 °C  
Rate = 300,300 lbs/hr



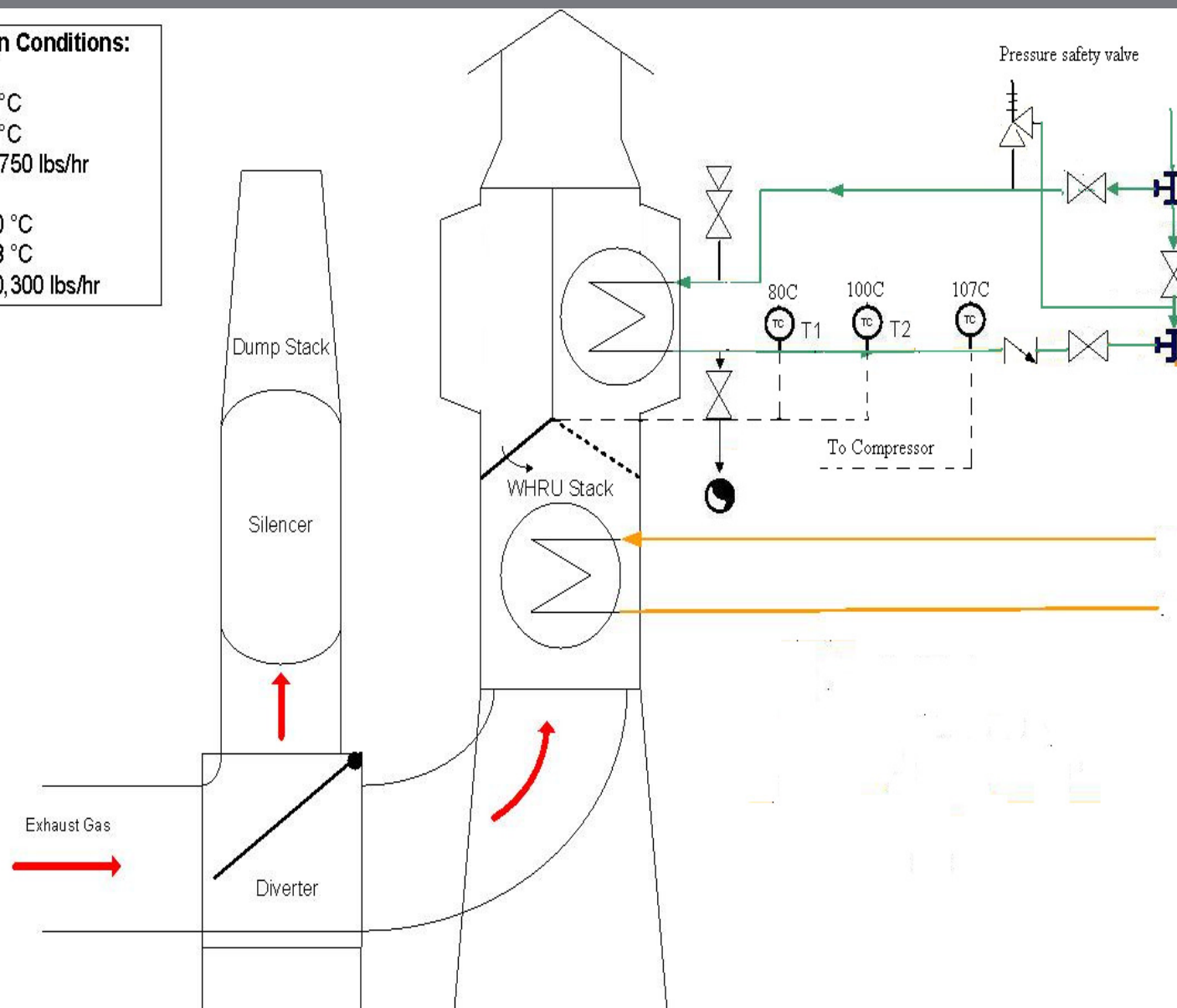


# WHRU Design – Final Design

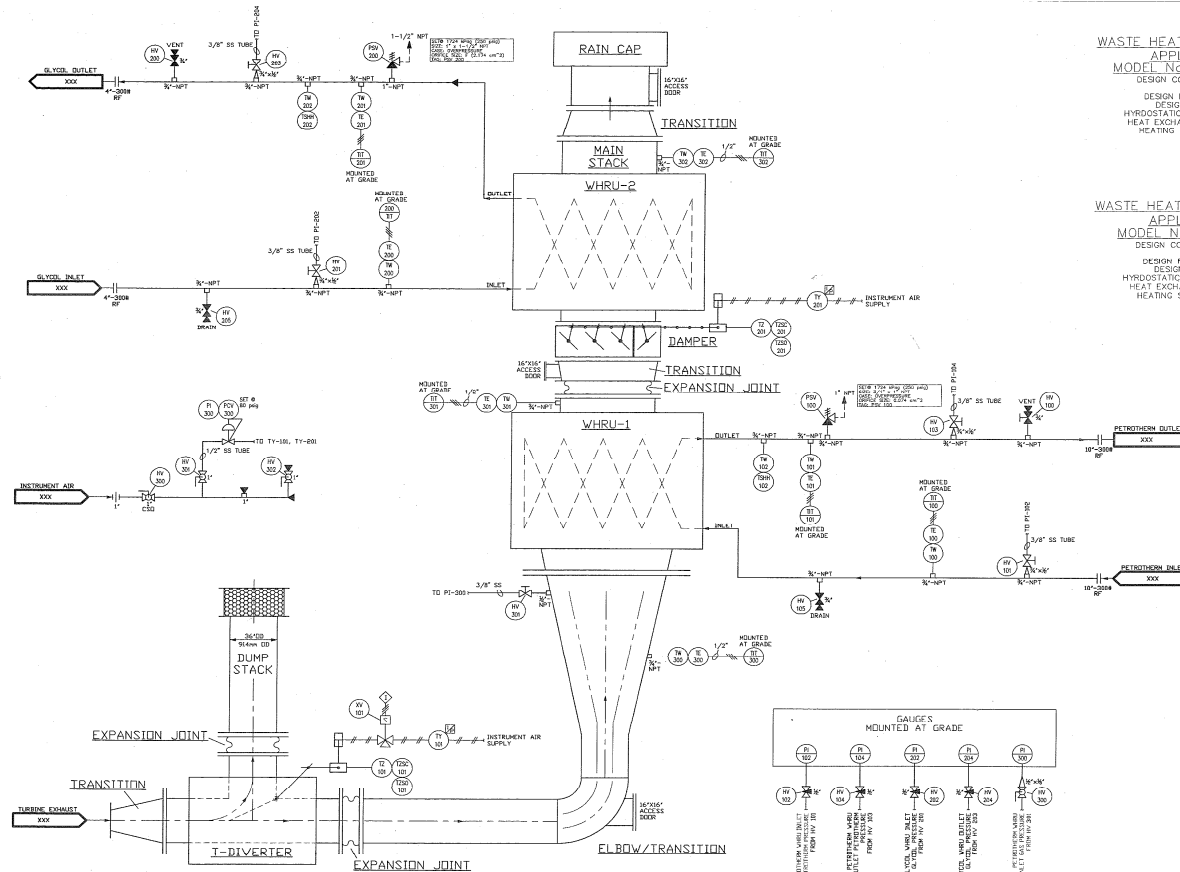
## Proposed Design Conditions:

Glycol In = 40 °C  
Glycol Out = 78 °C  
Rate = 50,750 lbs/hr

Hot Oil In = 160 °C  
Hot Oil Out = 178 °C  
Rate = 300,300 lbs/hr



# WHRU Design – Final Design



**WASTE HEAT RECOVERY UNIT-(WHRU-1)**  
**APPLIED HEAT RECOVERY**  
**MODEL No.: HOT OIL 10-300# 1/0**  
 DESIGN CODE: ASME SECTION I, 2007 EDITION  
 TYPE: FIN / TUBE  
 DESIGN PRESSURE: 1,724 kPaG [250 psig]  
 DESIGN TEMPERATURE: 343°C [650°F]  
 HYDROSTATIC TEST PRESS.: 2,586 kPaG [375 psig]  
 HEAT EXCHANGED: 1,874 kW [6,400,000 BTU/Hr]  
 HEATING SURFACE: 715 SQM [7,692 SQ.FT.]  
 CRN: U7590.2

**WASTE HEAT RECOVERY UNIT-(WHRU-2)**  
**APPLIED HEAT RECOVERY**  
**MODEL No.: GLYCOL 4-300# 1/0**  
 DESIGN CODE: ASME SECTION I, 2007 EDITION  
 TYPE: FIN / TUBE  
 DESIGN PRESSURE: 1,724 kPaG [250 psig]  
 DESIGN TEMPERATURE: 343°C [650°F]  
 HYDROSTATIC TEST PRESS.: 2,586 kPaG [375 psig]  
 HEAT EXCHANGED: 878 kW [3,000,000 BTU/Hr]  
 HEATING SURFACE: 773 SQM [8,323 SQ.FT.]  
 CRN: U7594.2

**ORIGINAL**  
 FEB 27 2009 HTH ES

REFERENCE DRAWINGS	GENERAL NOTES	REVISIONS	CUSTOMER TAG NO.	CUSTOMER PROJECT NO.	CUSTOMER PO NO.	DATE	BY	DESCRIPTION	DATE	NO.	BY	DESCRIPTION	DATE	NO.	BY	DESCRIPTION	DATE	NO.	BY	DESCRIPTION	DATE
100-606-42 GENERAL ARRANGEMENT	1.																				
SHOP CODE: N/A	THIS DOCUMENT CONTAINS MATERIAL AND/OR INFORMATION WHICH IS PROPERTY OF HTH HEATECH INC. AND SUPPLIED ONLY ON A CONFIDENTIAL BASIS. NO TRANSMITTAL OR DISCLOSURE SHALL BE MADE TO ANY PERSON, FIRM OR CORP. WITHOUT THE PRIOR WRITTEN APPROVAL OF HTH HEATECH INC.																				

**HEATECH**

HTH HEATECH INC.  
 CALGARY, ALBERTA, CANADA

PROCESS & INSTRUMENTATION DIAGRAM

END USER/CUSTOMER

TALISMAN ENERGY INC.

PROJECT/LOCATION

GAS TURBINE HEAT RECOVERY

DICTIONARY, AB

SCALE

DRAWING NO.

300-606-42

REV 0

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# Controls

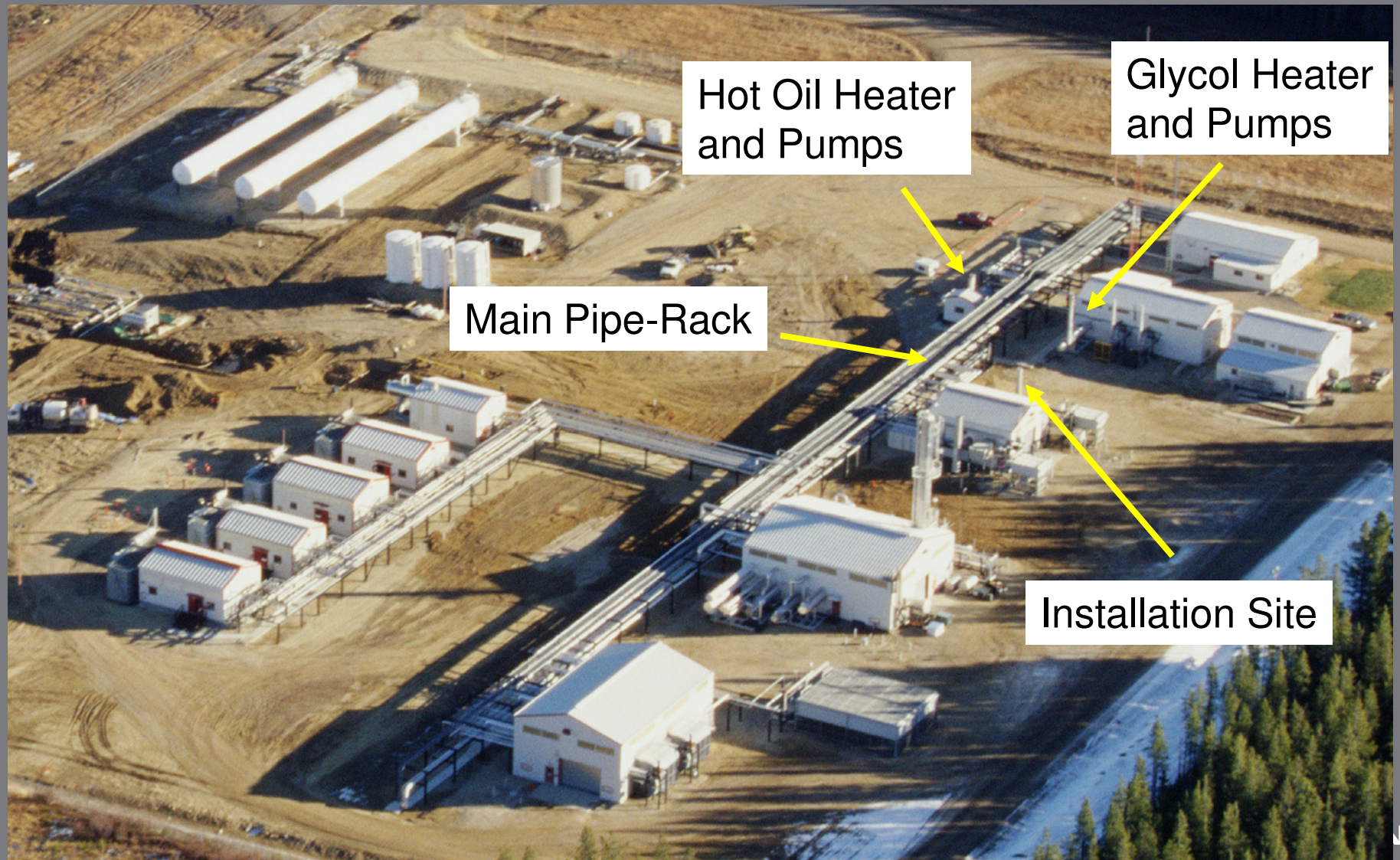
- Heat input into each thermo fluid needed to be controlled due to the extreme difference in operating temperatures
- Heat transferred to the hot oil and glycol controlled by exhaust flow through the WHRU Stack
- Exhaust flow is controlled by the main diverter for both fluids, glycol also secondarily controlled by additional damper
- Both fluids heated so that they reach optimum temperature as they return from the process
- Both fluids continue to run through existing fired line heater for additional heating if needed
- Both exchangers installed with high temperature protection and low flow protection, incorporated into the plant shutdown key
- Fire detection shutdown in stack (would be the result of ruptured tube)

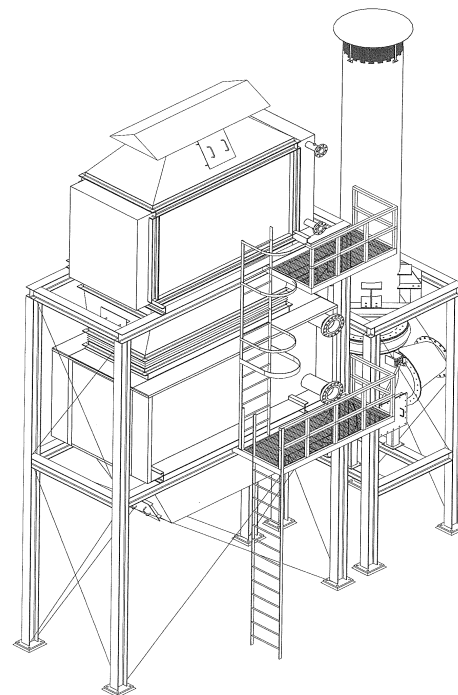
# Challenges

- Incorporating the 2 fluids with different properties into one WHRU unit, presented unique control problems.
  - Installed damper on glycol system to provide secondary control
- Purge time of the WHRU stacks, went from 30 seconds to 5 minutes
  - Installed new starters to handle the incremental time
  - Tied starters into flare system
  - Installed burst plate in system
- Control system presented unique challenges
  - Lots of Hazop meetings to ensure that we provided proper protection
  - Installed many layers of protection




# Installation- Site layout





ISOMETRIC VIEWS  
SCALE N.T.S.

REFERENCE DRAWINGS		GENERAL NOTES		REVISIONS				CUSTOMER TAG NO.			
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								DATE: 08-09-15			
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# Installation

- Took advantage of previous outage to install all hot oil/glycol tie-in connections
- Installed WHRU complete with pilings, associated piping, and all instrumentation while Plant was on line
- Took advantage of scheduled outage to complete the final tie-ins which included :
  - Removing turbine exhaust stack and installing transition piece to connect WHRU to turbine exhaust
  - Commissioning of the EI Systems
  - Installed new Solar Turbine Starters and tied the starter exhaust into the flare system



# WHRU Picture



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# WHRU Picture



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## Summary – Benefits/Impact

- Utilization of Solar Turbine Sales Compressor exhaust waste heat to heat process liquids
- Replaces existing hot oil and glycol heat mediums, allows 2 line heaters to be shut in
- Maintains heat in buildings during winter by maintaining glycol temperature
- Reduction in fuel gas usage of 0.3 mmscf/day
- CO<sub>2</sub> reduction of 5,900 t/y
- N<sub>2</sub>O reduction of 0.10 t/y
- Capital cost of \$875k, payout of 2.0 years based on a fuel gas cost of \$4.00 /mcf
- Potential of adding twin unit on 2nd Solar Turbine Compressor
- WHRU minimizes our environmental impact

# Future Considerations

- Technology can be utilized elsewhere now that it has been proven
- This design could be added to the 2<sup>nd</sup> Solar Turbine Compressor at Bigstone if an application is identified
- Installation costs can be reduced due to having the upfront Engineering done— cost could range from \$0.5 mm to 1.0 mm depending on application
- Future Turbine/ Centrifugal Compressor installs could be justified based on installing WHRUs
- Reciprocal Compressor Applications -- Further research needed

# Questions?

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**Thanks to the following people for  
their contributions and advice**

Dave Pillage (Project Supervisor)  
Yin Yanhua (Coop Student)  
Liam Russel (Coop Student)  
John Foxcroft (WP Engineering)  
Noel Charchuk (Heatech)  
Doug Kinas (Solar Turbine)

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